# LNG Safety

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# Education and experience

- BS & MS in Engineering Univ. of Michigan
- Licensed Professional Engineer California
- PhD in Applied Science Univ. of California, Davis
- Worked for LLNL for 36 years, recently retired.
- Helped create and manage Liquefied Gaseous Fuels Program
- Managed joint projects with
  - Oil company participants including AMOCO, Shell, Exxon, etc.
  - Gas Research Institute
  - US Coast Guard
  - Other companies and government agencies
- Expert witness at trials
- Congressional testimony on transport of hazardous materials
- California legislative testimony on safety of refineries
- Conducted vulnerability assessments at refineries after 9/11
- Member of team of independent consultants reviewing LNG import terminal proposed for Vallejo, CA
- Currently consulting on LNG safety analysis with BHP Billiton, Sandia
   National Laboratory and others

# What is LNG?

- Liquefied natural gas (LNG) is a cryogenic liquid and is mostly liquid methane
  - Density: 26.5 lb/ft³ (424 kg/m³) lighter than water
  - Boiling point: -260 °F (-162 °C)
- Natural gas is lighter than air and rises
- Vaporized LNG/air mixtures from spills are heavier than air because they are cold
- Natural gas is flammable between 5% (LFL) and 15% (UFL) by volume in air
- Combustible mixtures will detonate in confined spaces

# What can cause an LNG spill?

- Collision with another ship
- Ship grounding or striking
- Terrorist attack
- Sabotage by insider
- Operations or unloading accident
- Natural disaster earthquake, tsunami
- Leak
- Airplane collision

# What happens when LNG spills?

- Forms a pool
- Vaporizes rapidly, faster on water than on land
- Forms a vapor/air cloud that is heavier than air and moves downwind
- If vapor cloud encounters an ignition source, it will burn back to source and form a pool fire
- Vapor cloud can explode if confined
- On water, it can undergo rapid phase transition
- This explosive boiling produces a damaging shock wave but does not involve combustion
- It can cause brittle fracture of carbon steel ship structures

# In 1977 DOE/DOT initiated an LNG safety research program with these objectives

- Perform research necessary to understand, predict, and mitigate the consequences of large releases of LNG and other hazardous gases
- Evaluate and develop as needed computer models capable of predicting these consequences
- Conduct field tests to obtain required data
- Work closely with industry and government to solve specific problems

# Why was this research program needed?

- Prof. J. Haven's 1977 USCG report cited model LFL distances from 0.75 mi to 50 mi for a catastrophic 25,000 m³ LNG spill
- The Oxnard/Port Hueneme 1977 Safety and Site Analysis used these model results to estimate that a catastrophic 100,000 m³ LNG spill from an import terminal storage tank would yield LFL distances from 3 mi to 127 mi
- Something needed to be done to reduce this uncertainty

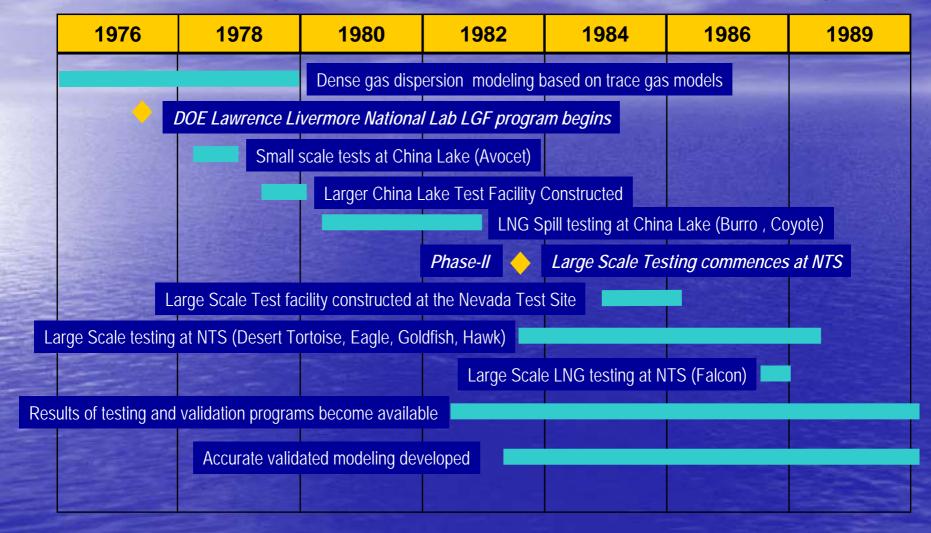
# Large scale testing was the first priority

- Large scale testing commenced in the 1980's
- Testing began simultaneously both in the US and the UK
- Models and predictions prior to that time varied greatly and accuracy was unknown
- Many scientific principles governing spills and dense gas dispersion in the atmosphere were not known or verified
- Scaling laws for large spills were not known

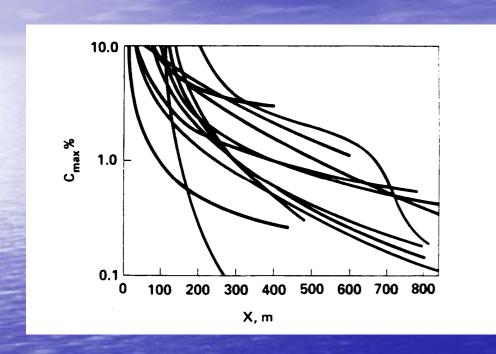
# Large scale field experiments in the '80s

name	year	material	no.	size m <sup>3</sup>	rate m <sup>3</sup> /min	purpose	sponsor
Maplin	1980	LNG, LPG	34	5 -31	1 - Inst	Dispersion, Combustion	Shell
Burro	1980	LNG	8	24-39	12-18	Dispersion	DOE
Coyote	1981	LNG	18	3-28	6-19	Combustion, RPT	DOE
Thorney Island	1982 1983 1984	Freon	43	2000 (gas)	Inst - 300	Dispersion, Obstacles	UK HSE
Desert Tortoise	1983	Ammonia	4	15-60	7-10	Dispersion	USCG, TFI
Eagle	1983	$N_2O_4$	6	1-4	0.5-2	Dispersion, Source	USAF
Goldfish	1986	HF	6	4	0.1-2	Dispersion, Mitigation	Amoco
Falcon	1987	LNG	5	20-66	9-30	Model Validation	GRI, DOT
Hawk	1988	HF	88	0.2	0.02	Mitigation	Mobil

# Time line for scientific experimentation and model validation conducted through DOE LLNL Liquid Gaseous Fuels Program



# By 1983 model predictions of HSE dense gas trials still varied by more than a factor of 100



- Pretrial dispersion model predictions of instantaneous release of Freon (2x air density)
- Simple, small release.
- Isothermal, flat terrain, no chemical reactions, no thermodynamic effects

- •Early model predictions were not based on adequate understanding of dense gas dispersion in the atmosphere
- The scientific basis was developed through experiments and models during the 1980's

# Coyote LNG vapor cloud burn experiment, China Lake, 1981

## **Poolfires**



# Regression rates for poolfires on land or water

- Burn on insulating concrete
  - Reg rate =  $3.3x10^{-4}$ m/s
    - $= 0.14 \text{ kg/m}^2\text{s}$
- Vaporization only on water
  - Reg rate =  $4x10^{-4}$ m/s =  $0.17 \text{ kg/m}^2$ s
  - Burn on water (sum above)
    - $\text{Reg rate} = 7.3 \times 10^{-4} \text{m/s}$ 
      - $= 0.31 \text{ kg/m}^2\text{s}$

# Rapid phase transition (RPT) explosions

- RPTs involve the explosive release of energy associated with boiling
- Rapid phase change not combustion
- They occur when a cold liquid is immersed in a hot liquid and heated to its superheat limit
- At the superheat limit, the cold liquid spontaneously and explosively vaporizes
- RPT accidents occur in metal foundries and the paper pulp industry also

# RPTs can be dramatic and damaging



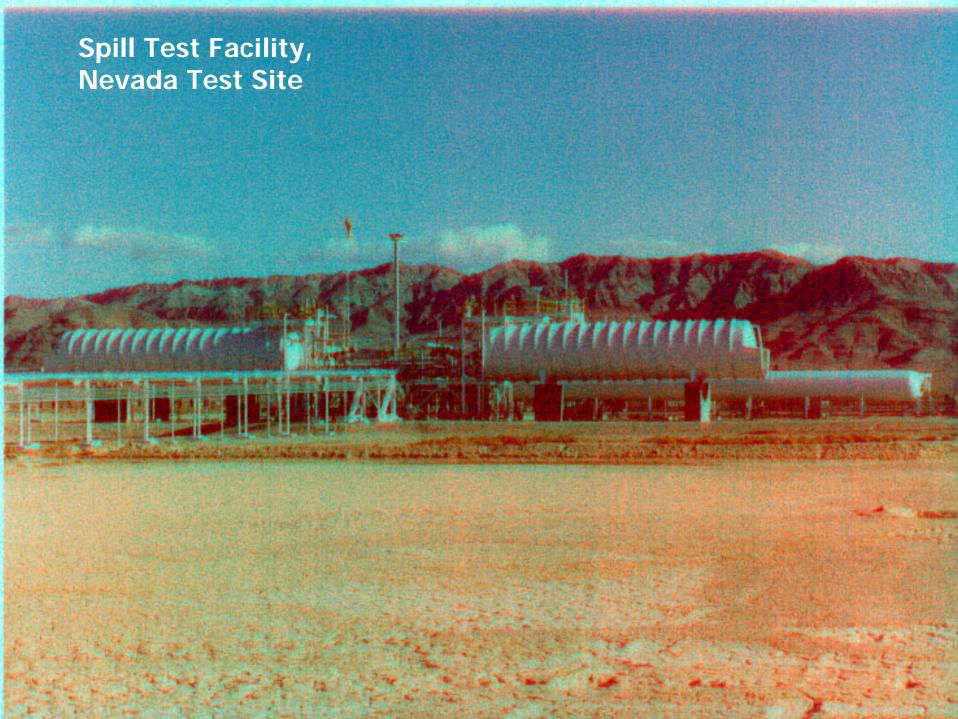
### Burro 9 RPT data 83% methane

Time <sup>a</sup> (s)	Side-on Pressure <sup>b</sup> (psi)	TNT equivalent <sup>c</sup> (g)
6.5	0.12	36
7.1	0.15	64
9.2	0.27	295
21.4		1890
35.1	0.72	3500
43.2	0.10	23
46.0	0.12	36
54.1	0.12	36
54.9	0.13	45
66.9	0.19	120
72.7	0.12	36

at = 0 is start of spill-valve opening.

<sup>&</sup>lt;sup>b</sup>Measured at distance of 30 m.

<sup>&</sup>lt;sup>c</sup>Equivalent free-air point-source explosion of TNT.





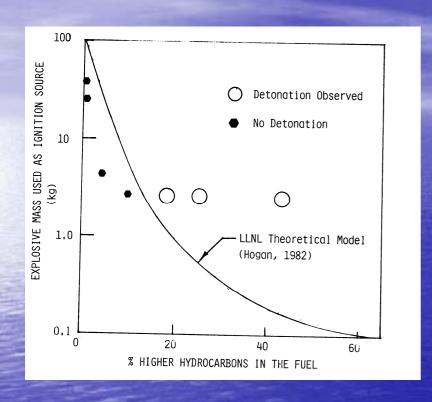
### Fireballs



Fireball from accidental ignition of Falcon5 LNG test in 1987

- Fireballs form when a rich compact vapor cloud is ignited. The hot spot rises, creating a vortex that rapidly incorporates the rest of the fuel
- They burn in seconds releasing a large amount of radiant energy
- They are common for propane and butane but not LNG

# Vapor cloud explosions and detonations



Detonation threshold NWC data with LLNL model for stoichometric fuel-air mixtures

- Unconfined ordinary LNG vapor clouds burn but do not detonate
- At higher hydrocarbon levels of 40% or more detonations can occur in unconfined clouds
- Detonations can always occur when vapor clouds are confined by walls, buildings, equipment racks or terrain

# What did the LGF program produce?

- Extensive scientific data on LNG spill and dense gas behavior for model development and validation
- Models to accurately predict the consequences and behavior of LNG and other dense gases
- A facility for large scale experiments

The ultimate product was confidence that the modeling programs and techniques were based upon good science, observation, measurement, and understanding of actual behavior.